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(54) Title: AMORPHOUS PRECIPITATED SILICA (57) Abstract Amorphous precipitated silica which may be used to form battery separators of very low shrinkage is characterized by (a) a BET surface area in the range of from 60 to 200 m ² /g; (b) a CTAB surface area in the range of from 40 to 150 m ² /g; (c) a DBP oil absorption in the range of from 180 to 300 cm ³ /100g; (d) a mean ultimate particle size in the range of from 20 to 30 nm; (e) a total intruded volume in the range of from 2.5 to 4 cm ³ /g; (f) an intruded volume in the range of from 0.3 to 1.2 cm ³ /g for pores having diameters in the range of from 20 to 100 nm; and (g) a pore diameter at the maximum of the volume pore size distribution function in the range of from 30 to 200 nm.		

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AMORPHOUS PRECIPITATED SILICA

The use of amorphous precipitated silica as a component of microporous polymeric battery separators is known. See, for example, United States Patents No. 3,351,495; 3,696,061; 3,798,294; 4,024,323; 4,210,709; 4,237,083; 4,331,622; 4,335,193; 4,648,417; 4,681,750; and 4,734,229. A characteristic of great importance to battery separators is that of high dimensional stability. The dimensional stability of a battery separator is determined by many factors including but not limited to the identities and proportions of materials of construction, the physical dimensions of which thickness is especially important, the porosity, and the types and numbers of the pores.

An amorphous precipitated silica has now been found which may be used to form battery separators of very low shrinkage. Accordingly, the invention is amorphous precipitated silica characterized by (a) a BET surface area in the range of from 60 to 200 m²/g; (b) a CTAB surface area in the range of from 40 to 150 m²/g; (c) a DBP oil absorption in the range of from 180 to 300 cm³/100g; (d) a mean ultimate particle size in the range of from 20 to 30 nm; (e) a total intruded volume in the range of from 2.5 to 4 cm³/g; (f) an intruded volume in the range of from 0.3 to 1.2 cm³/g for pores having diameters in the range of from 20 to 100 nm; and (g) a pore diameter at the maximum of the volume pore size distribution function in the range of from 30 to 200 nm.

Although both are silicas, it is important to distinguish amorphous precipitated silica from silica gel inasmuch as these different materials have different properties. Reference in this regard is made to R. K. Iler; The Chemistry of Silica, John Wiley & Sons, New York (1979), Library of Congress Catalog No. QD 181.S6144. Note especially

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pages 15-29, 172-176, 218-233, 364-365, 462-465, 554-564, and 578-579.

Silica gel is usually produced commercially at low pH by acidifying an aqueous solution of a soluble metal silicate, customarily sodium silicate, with acid. The acid employed is generally a strong mineral acid such as sulfuric acid or hydrochloric acid although carbon dioxide is sometimes used. Inasmuch as there is essentially no difference in density between the gel phase and the surrounding liquid phase while the viscosity is low, the gel phase does not settle out, that is to say, it does not precipitate. Silica gel, then, may be described as a non-precipitated, coherent, rigid, three-dimensional network of contiguous particles of colloidal amorphous silica. The state of subdivision ranges from large, solid masses to submicroscopic particles, and the degree of hydration from almost anhydrous silica to soft gelatinous masses containing on the order of 100 parts of water per part of silica by weight, although the highly hydrated forms are only rarely used.

Amorphous precipitated silica is usually produced commercially by combining an aqueous solution of a soluble metal silicate, ordinarily alkali metal silicate such as sodium silicate, and an acid so that colloidal particles will grow in weakly alkaline solution and be coagulated by the alkali metal ions of the resulting soluble alkali metal salt. Various acids may be used, including the mineral acids and/or carbon dioxide. In the absence of a coagulant, silica is not precipitated from solution at any pH. The coagulant used to effect precipitation may be the soluble alkali metal salt produced during formation of the colloidal silica particles, it may be added electrolyte such as a soluble inorganic or organic salt, or it may be a combination of both.

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Amorphous precipitated silica, then, may be described as precipitated aggregates of ultimate particles of colloidal amorphous silica that have not at any point existed as macroscopic gel during the preparation. The sizes of the aggregates and the degree of hydration may vary widely.

Amorphous precipitated silica powders differ from silica gels that have been pulverized in ordinarily having a more open structure, that is, a higher specific pore volume. However, the specific surface area of precipitated silica as measured by the Brunauer, Emmett, Teller (BET) method using nitrogen as the adsorbate, is often lower than that of silica gel.

Variations in the parameters and/or conditions during production result in variations in the types of precipitated silicas produced. Although they are all broadly amorphous precipitated silicas, the types of amorphous precipitated silicas often differ significantly in physical properties and sometimes in chemical properties. These differences in properties are important and often result in one type being especially useful for a particular purpose but of marginal utility for another purpose, whereas another type is quite useful for that other purpose but only marginally useful for the first purpose.

The BET surface area of the amorphous precipitated silica of the present invention is from 60 to 200 square meters per gram (m^2/g). From 80 to 180 m^2/g is preferred. As used in the present specification and claims, the BET surface area of the amorphous precipitated silica is the surface area determined by the Brunauer, Emmett, Teller (BET) method according to ASTM C 819-77 using nitrogen as the adsorbate but modified by outgassing the system and the sample for one hour at 180 C.

The CTAB surface area of the amorphous precipitated silica of the present invention may vary, but in most instances the CTAB surface area is in the range of from 40 to 150 square meters per gram (m^2/g). Often the CTAB surface area is in the range of from 50 to 130 m^2/g . From 60 to 120 m^2/g is preferred. As used in the present specification and claims, the CTAB surface area of the amorphous precipitated silica is the CTAB surface area determined in accordance the following procedure: Using a top loader balance, 11.0 grams (g) of cetyltrimethylammonium bromide, also known as CTAB and as hexadecyltrimethylammonium bromide, [CAS 57-09-0] is weighed to the nearest one-tenth milligram and the weight expressed in grams, C, is recorded. The weighed CTAB is dissolved in distilled water and diluted with distilled water to 2 liters in a volumetric flask to form a standard CTAB solution which is stored in the dark for at least 12 days before use. Using a top loader balance, 3.70 grams of Aerosol® OT sodium di(2-ethylhexyl) sulfosuccinate [CAS 577-11-7] (American Cyanamid Co., Wayne, NJ) is weighed. The weighed Aerosol® OT sodium di(2-ethylhexyl) sulfosuccinate is dissolved in distilled water and diluted with distilled water to 2 liters in a volumetric flask to form a standard Aerosol® OT solution which is stored in the dark for at least 12 days before use. The useful storage lives of the standard CTAB solution and the standard Aerosol® OT solution are two months after preparation. Using a pipet, 10.0 milliliters (mL) of the CTAB standard solution is transferred to a 250 mL Erlenmeyer flask containing a stirring bar. Next, 30 mL chloroform, 50 mL distilled water, 15 drops of 0.02% bromophenol blue aqueous indicator solution, and one drop of 1N aqueous NaOH solution are added to the flask. With vigorous stirring but minimal splashing, the contents of the Erlenmeyer flask are titrated with the standard Aerosol® OT solution from a 50 mL buret.

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The titration is begun at a rapid drop rate (the stopcock is never wide open) down to about 25 to 30 mL and then more slowly, dropwise, to the end point which will occur at about 37.5 mL. The approach to the end point is characterized first by a milky blue color throughout. Then, as the end point is more closely approached, the bottom chloroform layer becomes a more intense blue and the top aqueous layer takes on a lilac or purple hue. Immediately before the end point, the whole mixture becomes visibly clearer (i.e., less "milky") and the bottom layer is seen as a very intense blue. Using a wash bottle, the inside of the flask is washed down with no more than 25 mL of distilled water. The stirrer speed is increased to resume vigorous mixing for efficient contacting of the two liquid phases. At least 10 seconds are allowed to elapse after each dropwise addition of titrant immediately prior to the endpoint. Stirring is stopped frequently to allow the phases to separate so that the analyst can become familiar with these color changes and then vigorous stirring is resumed. At the end point the bottom phase loses all color and displays a colorless or milky white appearance while the top phase is intensely purple. The procedure is performed at least two times and the average volume of standard Aerosol® OT solution used per titration, V_1 , is recorded. A 200 mL wide mouth glass bottle is tared and approximately 0.500 gram of silica sample (in the as-received state, not dried) is placed in the bottle and weighed to the nearest 0.1 mg. This silica sample weight, S , is recorded. One hundred milliliters of the standard CTAB solution is pipetted into the bottle and a stirring bar is carefully added. Using a 50 mL pipet, filling and delivering twice, is preferred as the liquid level is easier to control than with a 100 mL pipet. A cap is screwed on the bottle and the contents are stirred gently for 15 minutes without pH adjustment. A pH electrode is placed

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into the solution in the bottle and gentle stirring is resumed. The pH is adjusted to between 9.0 and 9.5 using 1N aqueous NaOH added dropwise; approximately 5 drops of the 1N NaOH solution are required before the pH stabilizes between 9.0 and 9.5. When the pH has been stabilized between 9.0 and 9.5, the top of the bottle is covered with aluminum foil or equivalent to retard evaporation loss. The mixture is stirred gently for one hour at pH 9.0 to 9.5. The silica-liquid mixture is transferred to centrifuge tubes, balancing them by weighing on a top loader balance. The mixture is centrifuged for 30 minutes to produce a clear centrifugate. Clear centrifugate is carefully withdrawn using a dropping pipet and transferred to a small glass bottle. Using a pipet, 10.0 mL of the centrifugate is transferred into a 250 mL Erlenmeyer flask containing a stirring bar. Next, 30 mL chloroform, 50 mL distilled water, and 15 drops of 0.02% bromophenol blue aqueous indicator solution are added to the flask. The contents of the Erlenmeyer flask are titrated with the standard Aerosol® OT solution from a 50 mL buret using the same procedure and to the same endpoint used in titrating the standard CTAB solution. The volume of standard Aerosol® OT solution used, V_2 , is recorded. A small glass bottle (less cap) is heated for 2 hours at 105°C in an oven and cooled in a desiccator. The weight is recorded to the nearest 0.1 milligram (mg). Approximately one gram of silica sample is added to the bottle and the weight is recorded to the nearest 0.1 mg. The bottle and the sample are heated in an oven for 2 hours at 105°C. The bottle containing the sample is removed from the oven, immediately capped, and cooled in a desiccator. When cooled to ambient temperature, the cap is removed and the weight of the bottle containing the sample is recorded to the nearest 0.1 mg. The tare weight of the bottle is subtracted from the sample weighings and the weight in

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grams of the silica before heating, A, and the weight in grams of the silica after heating, B, are recorded. The CTAB surface area (dry basis), A_{CTAB} , expressed in m^2/g , is calculated according to the formula:

5

$$A_{CTAB} = \frac{(V_1 - V_2) (C) (A) (28.92)}{(V_1) (S) (B)}$$

10 The DBP oil absorption of the amorphous precipitated silica of the present invention may vary widely. In many instances the DBP oil absorption is from 180 to 300 cubic centimeters per 100 grams ($cm^3/100g$). From 180 to 260 $cm^3/100g$ is preferred. As used in the present specification and
15 claims, DBP oil absorption of the particles is determined according to ASTM D 2414-93 using dibutyl phthalate [CAS 84-74-2] as the absorbate and a Type E Absorptometer with the procedure modified as follows: (1) a sample of silica weighing 12.5 ± 0.1 grams (g) which is not further dried is
20 introduced to the Type E Absorptometer, (2) the moisture content of another sample of the silica weighing between 10 and 11 grams is determined using an Ohaus® moisture balance (Ohaus Corporation, Florham Park, NJ) with settings at 160°C and 10 minutes, and (3) the DBP oil absorption is calculated
25 from the equation:

$$OA = 100V/S + 3.9(M - 1.7)$$

where:

30 OA is the DBP oil absorption, $cm^3/100g$,
 V is the volume of dibutyl phthalate used, cm^3 ,
 S is the weight of the silica sample, g, and
 M is the moisture content, percent H_2O by weight.

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The amorphous precipitated silica may be in the form of aggregates of ultimate particles, agglomerates of aggregates, or a combination of both. The mean ultimate particle size of the amorphous precipitated silica of the invention (irrespective of whether or not the ultimate particles are aggregated and/or agglomerated) may vary considerably, but usually it is in the range of from 20 to 30 nanometers (nm). From 24 to 27 nm is preferred. As used herein and in the claims the mean ultimate particle size is determined by ascertaining the diameters of at least 256 well-defined ultimate particles using transmission electron microscopy and then calculating the arithmetic mean of the diameters so ascertained.

The total intruded volume of the amorphous precipitated silica of the present invention may vary widely. In many cases, however, the total intruded volume is in the range of from 2.5 to 4 cubic centimeters per gram (cm^3/g). Preferably the total intruded volume is from 2.5 to 3.4 cm^3/g .

The intruded volume of the amorphous precipitated silica of the present invention for pores having diameters in the range of from 20 to 100 nanometers (nm) may also vary widely. In many cases the intruded volume for pores having diameters in the range of from 20 to 100 nm is in the range of from 0.3 to 1.2 cubic centimeters per gram (cm^3/g). Preferably the intruded volume for pores having diameters in the range of from 20 to 100 nm is from 0.4 to 0.8 cm^3/g .

The pore diameter at the maximum of the volume pore size distribution function for the amorphous precipitated silica of the present invention may vary widely. Usually the pore diameter at the maximum of the volume pore size distribution function is in the range of from 30 to 200 nanometers (nm). From 45 to 130 nm is preferred.

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Both intruded volumes and the volume average pore size distribution function of the amorphous precipitated silica are determined by mercury porosimetry using an Autoscan mercury porosimeter (Quantachrome Corp.) in accordance with the accompanying operating manual. In operating the porosimeter, a scan is made in the high pressure range (from about 103 kilopascals absolute to about 227 megapascals absolute). The total intruded volume is the total volume of mercury which is intruded into the amorphous precipitated silica during the high pressure scan described above divided by the mass of the amorphous precipitated silica constituting the sample under test. The other intruded volume is that for pores having diameters in the range of from 20 to 100 nm divided by the mass of the amorphous precipitated silica constituting the sample under test. The volume pore size distribution function is given by the following equation:

$$D_v(d) = \frac{P}{d} \frac{dV}{dP}$$

where:

$D_v(d)$ is the volume pore size distribution function, expressed in $\text{cm}^3/(\text{nm} \cdot \text{g})$;

d is the pore diameter, expressed in nm;

P is the pressure, usually expressed in pounds per square inch, absolute; and

V is the pore volume per unit mass, usually expressed in cm^3/g .

Where the data are continuous or substantially continuous (i.e., small intervals between successive values of P), $D_v(d)$ is determined by taking $\Delta V/\Delta P$ for small values of ΔP from either a plot of V versus P or preferably from the raw data. Each value of $\Delta V/\Delta P$ is multiplied by the pressure at the upper end of the interval and divided by the corresponding pore

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diameter. The resulting value is plotted versus the pore diameter. The value of the pore diameter at the maximum of the volume pore size distribution function is then taken from the plotted graph. Numerical procedures or other graphical
5 procedures for estimating dV/dP may be used when desired or when necessary due to large intervals between successive values of P .

The dimensional stability-imparting properties of the amorphous precipitated silica of the present invention
10 were determined using a standard battery separator formulation and a standard protocol for making a battery separator, as follows:

A dry mixture is formed by admixing the components in the amounts shown in Table 1 in a Henschel® high intensity
15 mixer.

Table 1

	<u>Component</u>	<u>Amount, percent by volume</u>
	Silica	76.1
20	UHMWPE (1)	6.6
	Lubricant (2)	0.1
	Antioxidant (3)	0.1
	Carbon Black/polyethylene (4)	0.4
25	(1) UHMWPE = Ultrahigh Molecular Weight polyethylene, GUR 413, Hoechst Celanese Corp.	
	(2) Petrac® CZ81, Synpro Corp.	
	(3) Irganox® B215, Ciba-Geigy Corp.	
30	(4) Polyblak® 1850, A. Schulman, Inc.	

The standard battery separator formulation is formed by admixing 83.3 parts by volume of the above dry mixture with 17 parts by volume of Shellflex® 3681 processing oil (Shell Chemical Co.) in a Henschel® high intensity mixer. The
35 final mixture is in the form of a free-flowing powder. The final mixture is fed to a C. W. Brabender conical counter-rotating twin screw extruder. The extruder length to diameter

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ratio is 17/1. The screw diameter at the feed port is 42 millimeters and at the discharge end of the extruder is 25 millimeters. The extruder barrel comprises three temperature zones. The extrusion mixture feed port is located
5 just prior to the first temperature zone. Additional Shellflex® 3681 processing oil is added to the first temperature zone during extrusion to bring the total oil content in the extruded product to from 64 to 65 percent by weight. An atmospheric vent is located in the second
10 temperature zone. Extrudate from the barrel discharges into a 10.15 centimeter wide sheet die having a 1.524 millimeter discharge opening. Screen packs are in 14/60/14 mesh. The extrusion temperature is 215°C. The throughput is 7.71 kilograms per hour. The extrudate is calendered at
15 3.66 meters per minute to a sheet 0.203 millimeter thick and 15.24 centimeters wide. the extruded sheet is allowed to cool.

The cooled sheet is then die cut to rectangular sheets 12.7 centimeters long (machine direction) and
20 11.4 centimeters wide (cross direction). The rectangular sheets are extracted to equilibrium in a mixture of 12 weight percent Shellflex® 3681 processing oil and 88 weight percent n-hexane and then air dried at room temperature.

The length and width of the dry rectangles are
25 measured in three approximately equally spaced locations in each direction. An average (M_1) of the three measurements of the length (machine direction) is determined. An average (C_1) of the three measurements of the width (cross direction) is also determined. The measured rectangles are soaked for one
30 hour in room temperature water and then air dried at room temperature in a hood. The rectangles are remeasured in both directions as before and corresponding averages (M_2 and C_2 , respectively) are determined. Machine Direction Shrinkage (MD

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Shrinkage) and Cross Direction Shrinkage (CD Shrinkage), expressed as percent, are calculated as follows:

$$\text{MD Shrinkage} = \frac{M_1 - M_2}{M_1} \times 100$$

$$\text{CD Shrinkage} = \frac{C_1 - C_2}{C_1} \times 100$$

Inasmuch as these values are obtained under standard conditions, they are characteristics of the amorphous precipitated silica used in the battery separator formulation.

The Machine Direction Shrinkage may vary, but it is preferred that this value be low. In most instances the precipitated silica of the present invention is characterized by an MD Shrinkage of less than 3 percent. Preferably the MD Shrinkage is less than 2 percent.

The Cross Direction Shrinkage may vary, but it is preferred that this value also be low. Usually the precipitated silica of the present invention is characterized by a CD Shrinkage of less than 3 percent. Often the CD Shrinkage is less than 2 percent. Preferably the CD Shrinkage is less than 1 percent.

The amorphous precipitated silica of the present invention may be made by a process comprising:

(a) establishing an additive aqueous sodium silicate solution containing from 50 to 120 grams Na_2O per liter and having an $\text{SiO}_2:\text{Na}_2\text{O}$ molar ratio of from 3 to 3.4; (b) establishing an initial aqueous sodium silicate solution containing from 50 to 120 grams Na_2O per liter and having an $\text{SiO}_2:\text{Na}_2\text{O}$ molar ratio of from 3 to 3.4; (c) adding ambient temperature water to a reactor having a primary agitator and a supplemental high speed agitator located near the site of acid addition;

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(d) when the water level in the reactor is high enough that agitation with the primary agitator is possible, adding initial aqueous sodium silicate solution and water to the reactor with agitation to establish a second aqueous sodium silicate solution containing from 1.5 to 7 grams Na₂O per liter and having an SiO₂:Na₂O molar ratio of from 3 to 3.4; (e) injecting live steam into the second aqueous sodium silicate solution to form a third sodium silicate solution at a temperature in the range of from 91°C to 100°C; (f) over a period of 90 minutes while maintaining the temperature in the range of from 91°C to 100°C, adding acid and additive sodium silicate solution with primary agitation and with supplemental high speed agitation at the site of acid addition, to the third aqueous sodium silicate solution such that the Na₂O concentration remains in the range of from 1.5 to 7 grams Na₂O per liter and such that from 2 to 26 times as much sodium silicate is added as was present in the third sodium silicate solution; (g) optionally aging the reaction mixture for from 0 to 130 minutes with the supplemental high speed mixer off; (h) starting the high speed mixer and adding acid until the pH of the reaction mixture is in the range of from 3 to 4.5; (i) filtering and washing to a final sodium sulfate concentration of 2 percent by weight or less on a dry weight basis; and (j) drying the washed amorphous precipitated silica.

The acid used in the process may vary widely. In general, the acid added in step (f) should be strong enough to neutralize alkali metal silicate and cause precipitation of silica. The acid added in step (h) should be strong enough to reduce the pH to desired values within the specified range. The acid used in the various acid addition steps may be the same or different, but preferably it is the same. A weak acid such as carbonic acid produced by the introduction of carbon

dioxide to the reaction mixture may be used for precipitation of silica, but a stronger acid must be used in step (h) when it is desired to reduce the pH to values below 7. It is preferred to use strong acid throughout the process. Examples
5 of the strong acids include sulfuric acid, hydrochloric acid, nitric acid, phosphoric acid, and acetic acid. The strong mineral acids such as sulfuric acid, hydrochloric acid, nitric acid, and phosphoric acid are preferred; sulfuric acid is especially preferred.

10 The washing of step (i) may be accomplished by any of the procedures known to the art for washing solids. Examples of such procedures include passing water through a filter cake, and reslurring the precipitated silica in water followed by separating the solids from the liquid. One
15 washing cycle or a succession of washing cycles may be employed as desired.

The drying of step (j) may be accomplished by one or more known techniques. For example, the precipitated silica may be dried in an air oven or in a vacuum oven. Preferably
20 the precipitated silica is dispersed in water and spray dried in a column of hot air. The temperature at which drying is accomplished is not critical, but the usual practice is to employ temperatures of at least 400°C. Generally the drying temperature is less than 800°C. In most cases drying is
25 continued until the precipitated silica has the characteristics of a powder. Ordinarily the dried precipitated silica is not absolutely anhydrous but contains adsorbed water (from 1 to 7 weight percent) in varying amounts, the latter depending partly upon the prevailing
30 relative humidity. Adsorbed water is that water which is removed from a sample of the silica weighing between 10 and 11 grams using an Ohaus moisture balance with settings at 160°C and 10 minutes.

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An optional step which may be employed is size reduction. Size reduction techniques are themselves well known and may be exemplified by grinding, pulverizing, and fluid energy milling.

5 The degrees of agitation used in the various steps of the invention may vary considerably. The agitation employed during the addition of one or more reactants should be at least sufficient to provide a thorough dispersion of the reactants and reaction mixture so as to avoid more than
10 trivial locally high concentrations of reactants and to ensure that silica deposition occurs substantially uniformly thereby avoiding gellation on the macro scale. The agitation employed during aging should be at least sufficient to avoid settling of solids to ensure that silica deposition occurs
15 substantially uniformly throughout the mass of silica particles rather than preferentially on those particles at or near the top of a settled layer of particles. The degrees of agitation may, and preferably are, greater than these minimums. In general, vigorous agitation is preferred.
20 The invention is further described in conjunction with the following examples which are to be considered illustrative rather than limiting, and in which all parts are parts by weight and all percentages are percentages by weight unless otherwise specified.

25

EXAMPLE

Stock aqueous sodium silicate solution was prepared containing about 70 grams Na_2O per liter and having an $\text{SiO}_2:\text{Na}_2\text{O}$ molar ratio of 3.2. A 100-liter reactor equipped
30 with steam coils for heating, an inlet for sodium silicate solution, an inlet for acid, an outlet, a primary agitator, and a supplemental high-speed agitator located near the site of acid addition, was charged with 50.1 liters of deionized

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water and 0.5952 kilogram of anhydrous sodium sulfate. With agitation provided by the primary agitator, the charged materials were heated to 80°C using the steam coils to provide a sodium sulfate solution. Over a period of 22.5 minutes and with agitation provided by the primary agitator, 4.871 liters of stock aqueous sodium silicate solution was added such that the concentration of Na₂O in the solution in the reactor was about 0.20 normal. The solution in the reactor was heated to 95°C using the steam coils. With both agitators running and over a period of 90 minutes, separate streams of 19.486 liters of stock aqueous sodium silicate solution and 1.1 liters of 96 weight percent aqueous sulfuric acid were added. Upon completion of the additions the supplemental high speed mixer was shut off and the reaction mixture was aged for 70 minutes at pH 9.6 while the temperature was maintained at 95°C. At the conclusion of the aging period the supplemental high speed mixer was started and 96 weight percent aqueous sulfuric acid was added at a rate of 11.74 milliliters per minute until the pH of the reaction mixture was 3.8. The resulting slurry was transferred to several large 32-centimeter diameter Buchner funnels and washed with deionized water until the Na₂SO₄ content on a dry basis was 0.14 percent by weight. The filter cakes were removed from the funnels and, together with a small amount of added water, were liquefied by agitation and spray dried. The product was particulate amorphous precipitated silica having the following physical characteristics:

	BET Surface Area	163 m ² /g
	CTAB Surface Area	66 m ² /g
	DBP Oil Absorption	244 cm ³ /100g
30	Mean Ultimate Particle Size	26 nm
	Total Intruded Volume	3.1 cm ³ /g
	Intruded Volume for Pores Having Diameters in the Range	

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	of from 20 to 100 nm	0.56 cm ³ /g
	Median Particle Size	6.1 μm
	Pore Diameter at the Maximum of the Volume Pore Size	
5	Distribution Function	120 nm
	Machine Direction Shrinkage	1.6%
	Cross Direction Shrinkage	0.9%

Although the present invention has been described
10 with reference to specific details of certain embodiments
thereof, it is not intended that such details should be
regarded as limitations upon the scope of the invention except
insofar as they are included in the accompanying claims.

CLAIMS:

1. Amorphous precipitated silica characterized
by:
- 5 (a) a BET surface area in the range of from 60 to
200 m²/g;
- (b) a CTAB surface area in the range of from 40 to
150 m²/g;
- 10 (c) a DBP oil absorption in the range of from 180
to 300 cm³/100g;
- (d) a mean ultimate particle size in the range of
from 20 to 30 nm;
- (e) a total intruded volume in the range of from
2.5 to 4 cm³/g;
- 15 (f) an intruded volume in the range of from 0.3 to
1.2 cm³/g for pores having diameters in the
range of from 20 to 100 nm; and
- (g) a pore diameter at the maximum of the volume
pore size distribution function in the range
20 of from 30 to 200 nm.
2. The amorphous precipitated silica of claim 1
further characterized by a Machine Direction Shrinkage of less
than 3 percent.
3. The amorphous precipitated silica of claim 1
25 further characterized by a Machine Direction Shrinkage of less
than 2 percent.
4. The amorphous precipitated silica of claim 1
further characterized by a Cross Direction Shrinkage of less
than 3 percent.
- 30 5. The amorphous precipitated silica of claim 1
further characterized by a Cross Direction Shrinkage of less
than 2 percent.

6. The amorphous precipitated silica of claim 1 further characterized by a Cross Direction Shrinkage of less than 1 percent.

7. The amorphous precipitated silica of claim 1
5 characterized by a CTAB surface area in the range of from 50 to 130 m²/g.

8. The amorphous precipitated silica of claim 1 characterized by

- 10 (a) a BET surface area in the range of from 80 to 180 m²/g;
- (b) a CTAB surface area in the range of from 60 to 120 m²/g;
- (c) a DBP oil absorption in the range of from 180 to 260 cm³/100g;
- 15 (d) a mean ultimate particle size in the range of from 24 to 27 nm;
- (e) a total intruded volume in the range of from 2.5 to 3.4 cm³/g;
- (f) an intruded volume in the range of from 0.4 to 0.8 cm³/g for pores having diameters in the
20 range of from 20 to 100 nm;
- (g) a pore diameter at the maximum of the volume pore size distribution function in the range of from 45 to 130 nm.
- 25 (h) a Machine Direction Shrinkage of less than 2 percent; and
- (i) a Cross Direction Shrinkage of less than 1 percent.

INTERNATIONAL SEARCH REPORT

 International application No.
 PCT/US97/06562

A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) : C01B 33/12

US CL : 423/335, 339

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 423/335, 339

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

NONE

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

NONE

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US, 4,681,750 A (JOHNSON ET AL) 21 July 1987 (21-07-87), see col. 5, line 34 to col. 6, line 29.	1-8
P	US, 5,605,569 A (BOYER ET AL) 25 February 1997 (25-02-97), see col. 3, lines 1-48.	1-8

☐ Further documents are listed in the continuation of Box C.
 ☐ See patent family annex.

* Special categories of cited documents:	*T	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
A document defining the general state of the art which is not considered to be of particular relevance	*X	document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
E earlier document published on or after the international filing date	*Y*	document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
L document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	*A*	document member of the same patent family
O document referring to an oral disclosure, use, exhibition or other means		
P document published prior to the international filing date but later than the priority date claimed		

Date of the actual completion of the international search

23 MAY 1997

Date of mailing of the international search report

23 JUN 1997

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